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Photocatalytic Concrete Pavements: Laboratory Investigation of NO Oxidation Rate Under Varied Environmental Conditions

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Keywords

photocatalytic pavement, air pollution mitigation, nitrogen oxides, titanium dioxide, photoreactor bench-scale study

Disciplines

Construction Engineering and Management

Comments

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1. Introduction

Within the United States, an estimated 48 million people live within 90 m of a four-lane (or larger) highway, railroad, or airport (Primary National Ambient Air Quality Standards for Nitrogen Dioxide: Proposed Rule, 2009). This population segment is susceptible to negative health effects associated with NO₂ exposure (Brauer et al., 2002; Brunekreef et al., 1997; Finkelstein et al., 2004; Garshick et al., 2003; Kim et al., 2004). Nitrogen dioxide (NO₂), a motor vehicle air pollutant, is regulated by the United States Environmental Protection Agency (USEPA). The agency's justification for this regulation has recently been confirmed with evidence from multiple epidemiologic studies associating short-term NO₂ exposure and adverse respiratory symptoms, particularly in children and those affected with asthma (USEPA, 2008b).

NO₂ falls within a group of highly reactive oxides of nitrogen commonly known as NO_x. Nitric oxide (NO) accounts for 95% of NO_x emissions (USEPA, 2001). This pollutant is freely oxidized to NO₂ in the atmosphere; hence, the efforts to abate NO₂ pollution target NO emissions. In fact, due to the high reactivity of the various NO_x species, USEPA assumes all NO_x in emissions estimates to be in the form of NO₂ (USEPA, 2001). USEPA employs various mechanisms in an effort to minimize NO_x exposure (e.g., improvements in public transportation, establishment of lanes for high occupancy vehicles, facilitating non-automobile travel, and promulgation of tailpipe NO_x emissions standards) (Clean Air Act, 2008; USEPA, 2007). NO_x mitigation strategies are not exempt from the law of diminishing marginal returns; therefore, in addition to efficiently applying conventional mechanisms, novel technologies should be considered. These technologies may yield higher levels of pollution reduction per dollar spent. Photocatalytic pavements represent one of these novel approaches. When exposed to sunlight and in the presence of a low concentration of water molecules, titanium dioxide (TiO₂) contained within these pavements generates hydroxyl radicals ($\bullet$ OH), a powerful oxidizing agent. These radicals promote the oxidation of a variety of organic and inorganic pollutants. Notably, the photocatalytic property of these pavements results in oxidation of NO_x to NO₃⁻ (Figure 1).

Figure 1. Photocatalytic oxidation of NO and NO₂ by pavement containing TiO₂ (partially adapted from Ballari et al., 2011).

Employment of these pavements as a mechanism to minimize the ambient concentration of NO in a targeted area will require an extensive development of what is known about NO oxidation rates under varied environmental conditions. In an effort to provide this new knowledge, various researchers have published accounts of laboratory studies that evaluated photocatalytic pavement specimens within a photoreactor, an experimental apparatus that allows for the control of various environmental conditions (Dylla et al., 2010; Hüsken et al., 2009; Murata & Tobinai, 2002). Independent environmental variables investigated have included NO concentration, irradiance, test gas flow rate, and relative humidity. Although material variables, such as TiO₂ concentration and type, will also play a role, environmental variable results presented to date have not brought about a consensus in terms of the range in NO oxidation rates that can be expected. Murata et al. (2000), Hüsken et al. (2009), and Ballari et al. (2011) each suggest that NO oxidation rates positively correlate with NO concentration in situations when the photocatalytic surface was not saturated by NO; however, for tests conducted at the same environmental

conditions (1.0 ppmv , $10 \text{ W}\cdot\text{m}^{-2}$, $3 \text{ L}\cdot\text{min}^{-1}$, $50\% \text{ RH}$) the range in oxidation rates was wide ($38\text{--}84 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$). Similarly, publications have noted a positive correlation between irradiance and oxidation rate, but at $10 \text{ W}\cdot\text{m}^{-2}$ calculated oxidation rates were $87 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$ for Murata et al. (2000) and $24 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$ for Hüsken et al. (2009). Both Murata et al. (2000) and Hüsken et al. (2009) observed a negative correlation between relative humidity and oxidation rate; however, at 50% relative humidity oxidation rates differed by $22 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$. These prior studies have assumed that water vapor from the atmosphere serves as both the source of $\bullet\text{OH}$ required for photocatalytic oxidation and the material which adsorbs on the surface and blinds photocatalytically active sites. Yet, given the porous nature of cementitious mixtures, water contained within a pavement could also serve as a $\bullet\text{OH}$ source and blinding material. At the time of placement, these pores can become filled with water. As hydration occurs and pores become filled with air, water that is available as a $\bullet\text{OH}$ source and blinding material decreases. Therefore, a decrease in moisture contained in the slab could lead to either an increase or decrease in the NO oxidation rate of the slab; however, no lab investigation has tested this hypothesis. Hüsken et al. (2009) observed a positive correlation between percent NO removal (as opposed to NO oxidation rate) and flow rate (slope of a linear fit was less than -10). This finding was also reported in Ballari et al. (2010), however in this case slope was only slightly less than -1 . Finally, a review of the fundamentals of heterogeneous catalysis indicates that, due to the fact that reactant adsorption is dependent on temperature, oxidation rate appears to be correlated with temperature (Herrmann, 2010). However, literature pertaining to photocatalytic pavements is both vague and contradictory in terms of the relationship between slab temperature and NO oxidation, with one source asserting that oxidation rate increases with an increase in temperature (Beeldens et al., 2011) and another reporting a decrease in oxidation rate with increased temperature (Chen & Chu, 2011).

Consequently, this study employed TX Active mortar slabs and a photoreactor to evaluate the change in NO oxidation rate that occurs with changes in NO concentration, irradiance, test gas flow rate, relative

humidity, decrease in slab moisture, or temperature. In instances when published photocatalytic pavement data existed, the data collected in this study was compared with data published by other researchers in order to draw conclusions in regards to the range of NO oxidation rates that could be expected and the variation that occurs between specimens.

2. Materials and Methods

2.1. Photocatalytic Mortar Slab Preparation and Cleaning

Three photocatalytic mortar slabs were used to evaluate this study's objectives. These slabs measured 152 mm (6 in) × 152 mm (6 in) × 25 mm (1 in). For this study, the researchers used a commercially-available cement that contains TiO₂ (TX Active, Essroc Italcementi Group, Nazareth, PA). Although, the TiO₂ content in this cement was not provided by the manufacturer, within patents governing photocatalytic cements, TiO₂ content ranges from 2–10% by mass (Paz, 2010). The proportions of the cement (TX Active or Type I), water, and fine aggregate (ASTM C778 standard sand, U.S. Silica Co., Frederick, MD) were recorded as 624 kg·m⁻³ (1052 lb·yd⁻³), 262 kg·m⁻³ (442 lb·yd⁻³), and 1412 kg·m⁻³ (2380 lb·yd⁻³) respectively. Given the cement proportion and the range in TiO₂ cement content above, estimated TiO₂ content of the mortar was 12.5–62.4 kg·m⁻³. Given the small volume of the slabs constructed, the mix did not include coarse aggregate. Except for the coarse aggregate, the relative proportions of materials used to manufacture the laboratory mortar slabs were similar to that of a pavement section placed at a field site, which will be evaluated in future research efforts (*citation removed to ensure blind review*). Particular care was taken to use the same water-to-cement ratio for both lab and field mixtures. During the placement process, a paste of water and photocatalytic cement coats aggregates and when hardened forms the surface that is exposed to pollutants. To manufacture the slabs, a two-lift procedure was used with equal volumes of a Type I cement bottom lift followed by a TX Active photocatalytic cement top lift. A possibility exists that excess vibration and surface finishing could draw water to the surface, thereby reducing the TiO₂ concentration. To minimize this possibility the material was consolidated by tapping the sides of the form

with a mallet and leveled with use of a screed. Following placement, a damp cloth and plastic sheet were laid over the slab surface for a 24-h curing period. Following this initial curing period, the slabs were removed from the forms and placed in a 100% relative humidity room for the duration of a 14-d curing period.

Prior to evaluating NO oxidation rates (described in Section 2.3), slabs were cleaned by immersion in water (Type I reagent grade) for 2 h and oven-dried at 60°C (140°F) for 20 h. This procedure was similar to that specified by the International Organization for Standardization (ISO) standard 22197-1:2007(E); this standard governs evaluation of NO removal by photocatalytic materials (ISO, 2007).

2.2. Experimental Apparatus

A flow-through poly(methyl methacrylate) (PMMA, i.e., plexiglass) photoreactor served as the primary component of the experimental apparatus. Figure 2 provides a schematic of the photoreactor, along with the NO test gas supply system, UV-A light source, and NO/NO_x monitor. The international standard, ISO 22197-1:2007(E), provided information on the construction and operation of the setup (ISO, 2007). The test gas supplied to the photoreactor was a mixture of breathing air (Grade D, Airgas USA, LLC, North Central Region, West Chicago, IL) and 51.6 ± 1% ppmv NO balanced in nitrogen (EPA protocol gas, Praxair, Inc., Danbury, CT) adjusted to a NO concentration of 0.11–1.0 ppmv, relative humidity of 10–70%, and flow rate of 1.5–5.0 L·min⁻¹. A UV-A light (XX-15BLB, Ultra-Violet Products, LLC, Upland, CA), directed at the UV-A-transparent optical window located at the top of the photoreactor, activated the photocatalytic properties of the mortar slab. The primary emissions spectrum peak from the light was 365 nm. At the location of the slab surface, the irradiance at 365 nm was measured to be 0.22–1.5 × 10¹ W·m⁻² using 365 nm UV sensor and radiometer (CX-365 and VLX-3W, Vilber Lourmat, Marne-la-Vallée, France). Except for instances when temperature was investigated as an independent variable, slab temperature was room temperature (approximately 22°C).

As displayed in Figure 3, within the reactor, 25 mm (1 in) wide PMMA spacers secured the slab's position and were set at a height that was either flush with or less than 2 mm below the slab surface. Within the 300 mm long reactor, the gas flowed over the slab through a cross section with a width of 150 mm (6 in) and a height (H) of approximately 6 mm (0.25 in). Turbulent airflow over the slab would introduce additional variability in the test. Using the approach detailed in Hüsken et al. (2009), Reynolds number (Re) was calculated to be 42.6 using an air kinematic viscosity of $1.54 \times 10^{-5} \text{ m}^2 \cdot \text{s}^{-1}$ ($1.66 \times 10^{-5} \text{ ft}^2 \cdot \text{s}^{-1}$) and an air flow rate of $3 \text{ L} \cdot \text{min}^{-1}$ ($0.8 \text{ gal} \cdot \text{min}^{-1}$). The length (L_d) for a parabolic velocity profile in the photoreactor was estimated to be approximately 27.1 mm (1.1 in) by the following equation: $L_d = 0.1 \cdot Re \cdot H$. The estimated length was slightly longer than the length of the PMMA spacers, which indicates that approximately 1.1% of the slab surface did not have a fully developed parabolic velocity profile. At $3 \text{ L} \cdot \text{min}^{-1}$, theoretical retention time of the test gas within the photoreactor was estimated to be 38 s. Theoretical retention time of the test gas in the volume above the slab at $3 \text{ L} \cdot \text{min}^{-1}$ was estimated to be 2.7 s.

Figure 2. Diagram of experimental apparatus (partially adapted from Ballari et al., 2011).

Figure 3. Photograph of photoreactor and mortar slab (optical window removed to facilitate viewing).

A NO/NO_x monitor, (Model 410 Nitric Oxide Monitor and Model 401 NO₂ Converter, 2B Technologies, Inc., Boulder, CO), completed the experimental apparatus. The monitor recorded the gas concentrations at 10 s intervals and was set to measure either NO or NO_x. Unlike chemiluminescence instruments, which detect the light produced when NO reacts with ozone (O₃), the Model 410 measures the change in UV absorbance at 254 nm when O₃ is consumed upon reaction with NO. UV absorbance is an absolute method; therefore, the analyzer requires calibration annually to correct for non-linearity that exists in the photodiode response and associated electronics.

2.3. Operational Procedure

Operation of the experimental apparatus was divided into two phases: parameter setting and testing. While in the parameter setting phase, the test gas flowed through the photoreactor; however, the slab was not irradiated by UV light. This phase was used to set airflow rate, relative humidity, and pollutant concentration and lasted for approximately 10 minutes. After adjusting parameters to desired values, gas flow was maintained through the photoreactor for a period sufficient to reach steady-state conditions.

The testing period comprised two steps during which the UV light was turned off and on and concentrations of NO and NO_x were measured. Figure 4 illustrates the UV on and off measurement cycle. Time to complete this cycle was limited to 60 minutes to minimize the possible influence of slab degeneration (e.g., due to the adsorption of reaction products) on collected data. Of note, a gap occurred between measurement of UV light on and off segments. The change in concentration that occurred when the light was turned on or off was not instantaneous. The period between measurements permitted time for concentration stabilization after each parameter change. In some instances, the time gap was not sufficient for concentration stabilization. When analyzing the data strings, these values were identified and removed. The study also did not evaluate adsorption of NO that could occur on the slab or on other surfaces within the photoreactor; rather, in similarity to other studies, this research focused on NO removal that occurred as result of irradiance by UV light (Ballari et al., 2011, Hüsken et al. 2009).

Figure 4. Typical NO/NO_x monitor data from testing procedure.

An alternative approach to test for photocatalytic oxidation is to measure NO concentration as the test gas first flows through a bypass line and then is diverted to flow through the photoreactor. With this approach a portion of the decrease in concentration that occurs as the gas flows through the photoreactor could be due to adsorption on the slab and dilution by air leakage. Measuring the difference in

concentration between UV-off and -on periods avoided these error sources and limits the source for a change concentration to photo-oxidation and photo-dissociation. To evaluate whether photo-dissociation occurred within the photoreactor, the researchers also evaluated a slab that was not manufactured with photocatalytic cement (see Control in Table 1). A two-tailed t -test, assuming unequal variances, did not find evidence of a significant difference between average UV-off and UV-on NO concentration at 90% confidence ($t=3.019$, $df = 4$, $p = 0.039$).

2.4. Variable Control and Measurement for Completed Tests

To evaluate the objectives listed above, the study collected data on the NO oxidation rates of photocatalytic mortar slabs under varied environmental conditions. In some cases, NO_x oxidation rates were also collected. The following environmental variables were considered: NO concentration ($C_{UV\ off}$), irradiance ($Irrad.$), test gas flow rate (Q), relative humidity (RH), decrease in slab moisture, and slab temperature ($Temp$). Table 1 presents values of these variables for the tests of NO concentration, irradiance, test gas flow rate, relative humidity, and slab temperature. For these tests, at the initial measurement (Test ID 0), all variables were set at the values specified by ISO 22197-1:2007(E) (i.e., $C_{UV\ off} = 1.0$ ppmv, $Irrad. = 10\ W\cdot m^{-2}$, $Q = 3.0\ L\cdot min^{-1}$, $RH = 50\%$). In subsequent tests, each independent variable was decreased or increased from the ISO-specified values in order to evaluate the change in NO and NO_x oxidation. To facilitate comparison to other published work, selected values of these variables were similar to values reported in said studies.

Table 1. Environmental conditions and results of tests completed.

		Environmental conditions									Results					
Test #	Slab ID	Description	C _{UV off}		Irrad.		Q	RH	Slab temp.	C _{UV on}				Oxidation rate		
			(ppmv)		(W·m ⁻² × 10 ¹)		(L·min ⁻¹)	(%)	(°C)	(ppmv)		(nmol·m ⁻² ·s ⁻¹)				
			NO _x		NO						NO _x		NO			
			κ	s	κ	s					κ	s	κ	s		
0		Control			1.1	0.00067	1.0	3.0	50	22 ⁱ			1.1	0.0033		0.36
0	1	Initial	1.0	0.0039	1.0	0.0046	1.0	3.0	50	22 ⁱ	0.71	0.0022	0.64	0.00054	34	42
1	1	Δ conc.	0.12	0.014	0.11	0.011	1.0	3.0	50	22 ⁱ	0.068	0.00062	0.043	0.0019	6.5	9.8
2	1	Δ conc.	0.31	0.013	0.30	0.010	1.0	3.0	50	22 ⁱ	0.19	0.00055	0.15	0.00063	15	19
3	2	Δ irradi.	1.0	0.0030	1.0	0.0036	0.22	3.0	50	22 ⁱ	0.93	0.00035	0.89	0.00030	7.5	10
4	2	Δ irradi.	1.0	0.0054	1.0	0.012	0.40	3.0	50	22 ⁱ	0.88	0.00030	0.83	0.00031	11	15
5	2	Δ irradi.	1.0	0.0015	1.0	0.0029	0.70	3.0	50	22 ⁱ	0.88	0.0011	0.82	0.0015	15	20
6	2	Δ irradi.	1.0	0.0060	1.0	0.0034	1.0	3.0	50	22 ⁱ	0.86	0.0012	0.79	0.00041	17	25
7	2	Δ irradi.	1.0	0.0049	1.0	0.0051	1.5	3.0	50	22 ⁱ	0.76	0.0013	0.69	0.0012	27	34
8	1	Δ Q	1.0	0.020	1.0	0.016	1.0	1.5	50	22 ⁱ	0.58	0.0018	0.51	0.00055	28	33
9	1	Δ Q	1.0	0.0075	1.0	0.0068	1.0	5.0	50	22 ⁱ	0.84	0.0036	0.79	0.00055	27	35
10	1	Δ RH	1.0	0.0054	1.0	0.011	1.0	3.0	10	22 ⁱ	0.55	0.0021	0.50	0.0017	59	64
11	1	Δ RH	1.0	0.0037	1.0	0.0041	1.0	3.0	20	22 ⁱ	0.59	0.0024	0.52	0.00083	52	61
12	1	Δ RH	1.0	0.0034	1.0	0.0044	1.0	3.0	70	22 ⁱ	0.80	0.0025	0.73	0.00069	23	28
13	3	Δ temp.			1.0	0.0003	1.0	3.0	20	55			0.72	0.0041		30
14	3	Δ temp.			1.0	0.0024	1.0	3.0	20	49			0.72	0.0049		31
15	3	Δ temp.			1.0	0.0005	1.0	3.0	20	44			0.78	0.0060		26
16	3	Δ temp.			1.0	0.0010	1.0	3.0	20	39			0.70	0.0022		25
17	3	Δ temp.			1.0	0.00073	1.0	3.0	20	36			0.69	0.0029		27
18	3	Δ temp.			0.92	0.0017	1.0	3.0	20	34			0.70	0.0016		22
19	3	Δ temp.			0.92	0.0013	1.0	3.0	20	32			0.73	0.0054		18
20	3	Δ temp.			0.92	0.0077	1.0	3.0	20	19			0.73	0.0079		19
21	3	Δ temp.			0.88	0.0019	1.0	3.0	20	21			0.71	0.0013		17
22	3	Δ temp.			0.94	0.0018	1.0	3.0	20	22			0.78	0.0022		16
23	3	Δ temp.			1.0	0.0018	1.0	3.0	20	7.1			0.85	0.0041		13
24	3	Δ temp.			1.0	0.0013	1.0	3.0	20	13			0.81	0.0021		16
25	3	Δ temp.			1.0	0.0011	1.0	3.0	20	15			0.81	0.0042		14

ⁱslab temperature not measured during test; room temperature assumed

190 *2.4.1. NO concentration, irradiance, test gas flow rate, and relative humidity*

191 Needle valves and a mass flow controller permitted control of NO concentration, test gas flow rate,
192 and relative humidity. To control irradiance the distance between the UV light and photoreactor optical
193 window was varied until the target value was observed on the radiometer at the height of the slab surface.

194 *2.4.2. Slab temperature*

195 Prior to evaluation in the photoreactor, a pre-cleaned slab (procedure in Section 2.1) was brought to
196 an initial temperature that was either above or below room temperature. To obtain this initial
197 temperature, a slab was placed in either an oven (60°C) or a refrigerator (2-4°C) for a period of 2 h. After
198 removal from the oven or refrigerator, the slab was immediately loaded into the photoreactor. An infrared
199 thermometer (15-077-966, Thermo Fisher Scientific, Waltham, MA) recorded temperature at 5 points on
200 the slab surface (the slab center and the center of each quadrant) immediately prior to and after
201 photoreactor evaluation. If slab temperature was greater than room temperature, photocatalytic
202 evaluation began after temperature recording. When slab temperature is less than the test gas
203 temperature (22°C), the possibility of water vapor condensation—which would blind photocatalytically
204 active sties—must be considered because this condensation would falsely indicate reduced photo-
205 activity. This error can be minimized by ensuring that the lowest slab temperature is substantially above
206 the dew point temperature of the test gas. To create a substantial difference between temperatures, the
207 researchers selected a 20% relative humidity for the test gas (dew point = -2°C). As a result, even if the
208 test gas air cooled 5°C as it flowed over a cool slab, relative humidity would only increase to 60% and
209 saturation of the test gas would not occur. To further minimize this potential error, the researchers
210 attempted to evaporate condensed water by using valves to reduce the test gas relative humidity to 0%
211 for a 10 minute period. Following this period, the UV light was turned on, relative humidity was increased
212 to the target value (20%), and photocatalytic evaluation began. The possibility exists that the effort to

avoid error by water condensation was unsuccessful. This possibility was evaluated by comparing the slope of the NO oxidation rate versus temperature line for observations below and above 22°C (Section 3.1.6). It must also be noted, that in this portion of the study, the researchers sought to ensure that water vapor density remained constant throughout the tests, rather than relative humidity. To achieve this goal, relative humidity was set in reference to the test gas temperature, which remained constant, rather than the variable slab temperature.

Additional NO oxidation rate evaluations were completed in succession as the slab temperature increased or decreased. Three sets of successive tests were recorded at the following temperature classifications: hot (32–55°C, Test IDs 13–19), warm (19–22°C, Test IDs 20–22), and cool (7.1–15°C, Test IDs 23–25) as shown in Table 1. Conducting successive tests could lead to a decrease in reactivity over time; therefore, the testing period was reduced such that the total testing time for the hot, warm, and cool classifications was 90, 40, and 40 minutes, respectively. Slab temperature was not measured at the midpoint of each test; instead, this value was estimated. The temperature and time data collected during the hot ($n = 40$), warm ($n = 20$), and cold ($n = 20$) sets of successive tests fit power law curves when adjusted for asymptotic values ($R^2 > 0.95$ for each set). For example, temperature for the hot classification was estimated using the following equation: $T = 5 \times 10^{-5} \cdot [(t + 647)/1440]^{-16.76} + 28$ ($T = \text{temperature in } ^\circ\text{C}, t = \text{elapsed time in minutes}, R^2 = 0.99$). These curves were used to estimate slab temperature at the midpoint of the photoreactor test.

2.4.3. Decrease in slab moisture

To evaluate the effect of a decrease in slab moisture, NO oxidation was periodically evaluated as water content decreased after starting at a saturated state. For these tests, NO concentration was set to 1.0 ppmv, flow rate to 3 L·min⁻¹, relative humidity to 20% and UV-A irradiance to 10 W·m⁻² at 365 nm. In similarity with the approach used in Section 2.4.2, a constant vapor density was ensured by setting relative

humidity in reference to the test gas temperature. To achieve saturation, a slab was immersed in water for 24 h. To promote a decrease in slab moisture, the slab was placed in a 60°C oven. The slab was periodically removed from this oven in order to measure slab mass and NO oxidation rate. Testing continued for the duration of 48 h. The decrease in slab moisture was presented as a percentage using the mass at the point of saturation and the calculated moisture loss (i.e., the difference in mass at saturation and at the point of photoreactor evaluation).

2.5. Presentation of Results

Other published works present NO removal as a percentage based on the difference between UV-off and -on concentrations of NO. Percent removal data is in part a function of lab setup (e.g., slab dimensions). Presenting results in this manner can lead to misperceptions if, for example, results are not normalized by area. In this research results are presented as the average NO oxidation rate in the reactor volume using the equation given by Minero et al. (2013):

$$NO \text{ oxidation rate} = \frac{P}{R \cdot T} \cdot \frac{Q}{A} \cdot C_{UV \text{ off}} \cdot \ln\left(\frac{C_{UV \text{ off}}}{C_{UV \text{ on}}}\right) = \left[\frac{nmol}{m^2 \cdot s}\right]$$

where,

$$P = \text{atmospheric pressure} = 101.3 \text{ kPa},$$

$$R = \text{ideal gas constant} = 8.314 \times 10^{-12} \text{ m}^3 \cdot \text{kPa} \cdot \text{nmol}^{-1} \cdot \text{K}^{-1},$$

$$T = \text{temperature} = [K],$$

$$Q = \text{volumetric flow rate} = [m^3/s]$$

$$A = \text{slab surface area} = 0.023 \text{ m}^2,$$

$$C_{UV \text{ off}} = \text{NO concentration with UV light off} = [ppmv], \text{ and}$$

$$C_{UV \text{ on}} = \text{NO concentration with UV light on} = [ppmv].$$

The recorded test gas temperature was used to calculate oxidation rate for evaluations of NO concentration, irradiance, flow rate, and relative humidity. Due to the low mass flow rate ($5.6 \times 10^{-5} \text{ kg}\cdot\text{s}^{-1}$) and specific heat of air ($1.007 \text{ kJ}\cdot\text{kg}^{-1}\cdot\text{°C}^{-1}$), evaluations of slab temperature and slab moisture assumed that the test gas temperature was the same as the slab temperature.

3. Results and Discussion

3.1. NO Oxidation Rate for Tests Completed

Table 1 documents the environmental parameters and oxidation rate results of the tests completed for this study. Of note, in each instance the value of NO oxidation rate is greater than that of NO_x oxidation rate. It could be expected that since the test gas supply to the reactor was nearly entirely comprised of NO, then the NO and NO_x removal values would be the same value. The discrepancy arises because NO is not oxidized completely to HNO₃. Rather, a portion of the gas is transformed to NO₂. NO₂ that remained in the gas stream was counted as part of the outlet NO_x concentration. As a result, NO_x removal measured lower than NO removal.

In this study, all slabs were prepared with the same procedure, materials, and proportions but in different batches. Review of Table 1 finds that although Tests IDs 0 and 6 were evaluated at the same environmental conditions, the observed NO oxidation rate differed by 51% from the mean. This difference may be due to several non-obvious factors within the mixing, placement, and curing steps. Prior research also indicated that oxidation rate differences may occur between slab replicates. For example, Hüsken et al. (2009) found that the percent difference of degradation rates for various replicates of photocatalytic pavement materials varied from as low as 0% to as high as 63%. Noting that differences did occur between slab replicates, Figures 5 to 9 plot each independent variable versus NO oxidation rate for a selected slab. To place this study's observations in context, overlaid on these plots are the data reported from previous

research that investigated NO oxidation rates under differing environmental conditions (Ballari et al., 2010; Ballari et al., 2011; Hüsken & Brouwers, 2008; Hüsken et al., 2009; Murata et al., 2000).

3.1.1. Influent NO Concentration

Figure 5 indicates a correlation between inlet NO concentration and NO oxidation rate ($R^2 = 0.994$). This correlation is also evident in the data from Murata et al. (2000) ($R^2 = 0.984$ for 0–1.0 ppmv, $R^2 = 0.802$ for 0–5.0 ppmv), Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($R^2 = 0.991$), and Ballari et al. (2010) ($R^2 = 0.882$).

Figure 5. Effect of influent NO concentration on NO oxidation rate.

A correlation between inlet concentration and NO oxidation rate was previously reported by Herrmann (1999). This publication indicated that kinetics follow a Langmuir-Hinshelwood mechanism, under which both reactants adsorb (e.g., NO and $\bullet$ OH) on the surface before a new molecule is formed. For these type of reactions, kinetics typically fell into low-concentration and high-concentration classifications. In the low-concentration classification, oxidation kinetics were first-order; whereas in the high-concentration classification, oxidation kinetics were zero-order. As applied to NO degradation by

photocatalytic pavements, this framework would indicate that, at high concentration, the rate of NO oxidation would remain constant. A constant oxidation rate occurred because a finite number of active sites were available for photocatalytic degradation. Once these sites were occupied, the rate of oxidation did not increase. In contrast, while within the low-concentration classification, the active sites had not yet been filled (Herrmann 1999).

For reactants adsorbed from aqueous phases, Herrmann (1999) indicated that a first-order kinetics apply when concentration is less than 10^{-3} M and zero-order kinetics apply at a concentration greater than 5×10^{-3} M. These divisions have not been established for reactants adsorbed from a gas phase. Except for Ballari et al. (2010), which only had 3 observations, *t*-tests of the data presented in Figure 5 rejected a null hypothesis that slope equaled $0 \text{ nmol m}^{-2}\cdot\text{s}^{-1}\cdot\text{ppmv}^{-1}$ ($p = <0.033$). Based on this analysis, it is evident that this data falls into first-order oxidation kinetics, indicating that active sites have not been filled. For applications of photocatalytic pavement, a determination of where the breakpoint between first- and zero-order oxidation kinetics occurs is not necessary. Locations where these pavements may be installed can be assumed to have NO_x concentrations near the National Ambient Air Quality Standards (NAAQSs) for NO₂ (i.e., 53 and 100 ppbv) (Primary National Ambient Air Quality Standards for Nitrogen Dioxide: Final Rule, 2010). These values are substantially below the 1.0 ppmv upper limit of the data analyzed; therefore, field applications can also be assumed to be characterized by first-order oxidation kinetics.

In addition to finding evidence that influent NO concentration affects NO oxidation rates, a *t*-test which compared the slope of linear regression lines for the presented data sets found no significant difference between this study's data and the data from Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t = -1.429$, $df = 3$, $p = 0.248$), and Ballari et al. (2010) ($t = -0.515$, $df = 2$, $p = 0.658$). A similar *t*-test did find that the slope was significantly different than the 0–1.0 ppmv data from Murata et al. (2000) ($t = -10.834$, $df = 4$, $p = 0.000$). Review of Murata et al. (2000)'s writing found that the reactor setup was not

markedly different than that of the authors'; therefore, material characteristics are also likely to influence the activity of photocatalytic pavements. More broadly, it can be concluded that because these slopes are significantly different, a generalized assumption of the effect of NO concentration on NO oxidation rate cannot be made. Instead, if a photocatalytic material is to be used in the field, it would be wise to complete lab evaluations in order to project levels of oxidation that could be observed in the field.

3.1.2. UV-A Irradiance

Figure 6 indicates a positive correlation between UV-A irradiance and NO oxidation ($R^2 = 0.996$). This correlation is also evident in the data from Murata et al. (2000) ($R^2 = 0.910$), Hüsken et al. (2009) ($R^2 = 0.940$), and Ballari et al. (2011) ($R^2 = 0.986$). This positive correlation exists because increased UV-A irradiance on a photocatalytic surface increases the rate at which electron holes are created. An increase in the rate of electron-hole generation results in the increased production rate of hydroxyl radicals, which oxidize NO. Multiple publications report that the relationship between irradiance and pollutant oxidation can be divided into two classifications. Although disagreement exists on the value of the division point between classes (10–250 $\text{W}\cdot\text{m}^{-2}$), the publications note a linear relationship below the division point and a non-linear relationship above this point (Herrmann et al., 2007; Jacoby et al., 1995; Kumar et al., 1995; Lim et al., 2000; Obee & Brown, 1995). Jacoby et al. (1995) explains that under the linear classification, electron holes are filled by reactions with species on the photocatalytic surface (e.g., OH^-) faster than by recombination with excited electrons; in contrast, under the non-linear classification, holes are filled by recombination at a faster rate than by reaction with other species.

Figure 6. Effect of UV-A irradiance on NO oxidation rate [Ballari et al. (2011) collected data at 0.52 ppmv inlet NO concentration, all other studies used a 1.0 ppmv inlet NO concentration].

As noted above, a linear relationship is apparent when reviewing the data collected in this study ($R^2 = 0.996$). Comparison of this data with Hüsken et al. (2009) did not find a significant difference in the slope of each data set's linear regression lines ($t = -0.403$, $df = 14$, $p = 0.693$). However, it should be noted that Hüsken et al. (2009) asserted power law relationship between percent NO removal and irradiance ($y = 8.583x^{0.431}$, $R^2 = 0.998$) and concluded that linear behavior was limited to observations above $4 \text{ W}\cdot\text{m}^{-2}$. Linear behavior is also apparent in Ballari et al. (2011) ($R^2 = 0.986$), but comparison of slopes did find a significant difference ($t = -8.462$, $df = 7$, $p = 0.000$). In contrast, the data from Murata et al. (2000) appears non-linear ($R^2 = 0.910$ for linear regression). Furthermore, a t -test comparing the slope of linear regression lines between this data set and the authors' found a significant difference ($t = -5.672$, $df = 7$, $p = 0.001$). In similarity with the conclusion reached in Section 3.1.1, this difference indicates that lab evaluation of a specific material selected for field application is warranted in order to assess its NO oxidation potential.

As reported by Grant and Slusser (2005), mean daytime UV-A irradiance ranged from 10.5 to 22.3 $\text{W}\cdot\text{m}^{-2}$ for the most northern and southern locations (Fairbanks, Alaska, latitude 65.1°N and Homestead, FL, latitude 25.4°N , respectively) according to the United States Department of Agriculture (USDA) climate

monitoring network. In addition to knowledge of the mean UV-A irradiance, application of photocatalytic pavement also requires knowledge on the change in irradiance during daylight hours. This knowledge is needed because in urban areas NO_x ambient concentration reportedly follows a diurnal pattern associated with traffic. Urban background monitoring in London, UK, found that NO_2 peaks both in early morning and late afternoon and NO , which oxidizes quickly to NO_2 during daylight hours, peaks in early morning (Bigi & Harrison, 2010). At these peaks, irradiance values are substantially lower than the mean daytime value. For example, at the 40th parallel north, which roughly runs through the center of the United States, the difference between the typical mid-summer peak UV radiation and the radiation 4 hours earlier in the day is more than 70% (Long et al., 1996). At present, oxidation rates at these low irradiance values are quite low. To be effective at peak pollution hours, the ongoing efforts by other researchers to enhance TiO_2 's photo-induced reactivity must be incorporated into new formulations of photocatalytic pavements.

3.1.3. Flow Rate

A model utility test on the data collected in this study (presented in Figure 7) did not reject a null hypothesis that slope equaled $0 \text{ nmol} \cdot \text{m}^{-2} \cdot \text{s}^{-1} \cdot ^\circ\text{C}^{-1}$ ($t = 0.118$, $df = 2$, $p = 0.925$), and therefore did not provide evidence of a correlation between flow rate and NO oxidation rate. The same conclusion was found with analysis of data from Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t = 0.631$, $df = 2$, $p = 0.642$). The independence of oxidation rate and flow rate aligns with the overall approach used by Hunger et. al (2010) to model the oxidation of NO on photocatalytic concrete surfaces. Using a Langmuir-Hinshelwood model and data collected with a photoreactor, Hunger et. al (2010) established that it is the conversion of adsorbed species that limits the reaction rate, rather than mass transfer from the test gas to the sample surface.

Figure 7. Effect of flow rate on NO oxidation rate.

Results, presented in the form of percent NO removal, were determined to be 51, 37, and 21% for flow rates of 1.5, 3, and 5 L·min⁻¹, respectively. Using these units, a negative relationship was evident between flow rate and percent removal ($t = -27.718$, $df = 2$, $p = 0.023$). This relationship was also documented by other researchers (Ballari et al., 2010; Dylla et al., 2010; Hüsken & Brouwers, 2008; Hüsken et al., 2009). These studies suggested that percent NO removal from a specific volume of test gas increases proportionally to the residence time over a photocatalytic surface because more time exists for pollutants to absorb and be oxidized at active sites. Overall, the lack of a correlation between flow rate and NO oxidation rate could simplify modeling efforts as stakeholders consider field applications. However, given the wide array of variables that need to be considered, this modeling effort will be challenging and is likely to have a high degree of uncertainty.

3.1.4. Relative Humidity

Figure 8 indicates a negative correlation between relative humidity and NO oxidation rate for the mortar slabs (created with cement that contains TiO₂) used in this study ($R^2 = 0.996$, $t = -22.257$, $df = 3$, $p = 0.002$). This correlation was also found in the study by Murata et al. (2000) ($t = -4.307$, $df = 5$, $p = 0.013$) and Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t = -22.408$, $df = 7$, $p = 0.000$). Photocatalytic

degradation of NO by pavement containing titanium dioxide occurs when NO is oxidized by $\bullet\text{OH}$ (Figure 1). These $\bullet\text{OH}$ are generated by oxidation of an OH^- by an electron hole. Current understanding proposes that water adsorbed on the slab serves as the source for OH^- . Intuition would thereby suggest that increased humidity would result in an increased rate of NO oxidation. By observation, the opposite has been found to be true. In addition to photocatalytic properties, materials containing TiO_2 also exhibit photo-induced superhydrophilicity (i.e., water on the surface has a contact angle of nearly 0°) (Fujishima et al., 2008). Adsorbed water vapor disperses over the surface, blinding photocatalytically active sites (Beeldens, 2007).

Figure 8. Effect of relative humidity on NO oxidation rate.

Although a negative correlation was found in each data set displayed in Figure 8, both data values and relationships differed. A null hypothesis that the difference in slopes of regression lines was 0 (i.e., $H_0: B_1 - B_2 = 0$) was used to compare this study's data to the data obtained by other researchers. This evaluation found a significant difference in slope between this study and both Murata et al. (2000) ($t = 2.859$, $df = 6$, $p = 0.029$) and Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t = -9.378$, $df = 8$, $p = 0.000$). Evaluation of the y-intercept found a significant difference between this study and both Murata et al. (2000) ($t = -423.737$, $df = 6$, $p = 0.000$) and Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t =$

978.105, $df = 8$, $p = 0.000$). This evaluation provides further evidence of the complexity of photocatalytic pavement materials. As concluded in previous sections, the researchers recommend that individual materials undergo a thorough evaluation prior to field evaluation.

The observed negative correlation that occurs as a result of water's blinding effect could limit the effectiveness of photocatalytic pavement in humid regions. Based on 2006–2008 data, the five counties with the highest ambient NO_2 concentration in the form of the 2010-promulgated NO_2 standard for counties within the United States are as follows: Cook, IL, San Diego, CA, Los Angeles, CA, Erie, NY, and Denver, CO (USEPA, 2010a). With the exception of Denver County, each of the listed counties frequently experiences high humidity conditions. As displayed in Figure 8, the NO oxidation rate at high humidity is substantially diminished. Unless photocatalytic pavements can be modified to lessen their sensitivity to changes in relative humidity, effective application in these polluted areas will be difficult.

3.1.5. Decrease in Slab Moisture

Figure 9 presents data obtained from a slab that was periodically removed from a 60°C oven and evaluated in the photoreactor as internal moisture decreased from a saturated state. For a decrease in moisture of 0–2% of saturated mass, a positive correlation is apparent ($R^2 = 0.822$) and a 0 slope null hypothesis was rejected ($t = 4.310$, $df = 5$, $p = 0.013$). Conversely, for a decrease in slab moisture greater than 2% of saturated mass, a negative correlation is apparent ($R^2 = 0.985$) and a 0 slope null hypothesis was rejected ($t = -14.152$, $df = 5$, $p = 0.001$). These observations can be explained as follows: between 0 and 2% decrease in moisture, as water is evaporated from the slab it no longer blinds active sites and the NO oxidation rate increases. This explanation is similar to the explanation for the correlation between relative humidity and NO oxidation rates. For a decrease in moisture above 2% the rate of NO oxidation appears to be limited because water contained within the slab is not available as a source for $\bullet\text{OH}$. While the primary purpose of these results is to indicate that slab moisture influences NO oxidation rate, it is

worth noting that these tests occurred at an average slab temperature of approximately 50°C. Data presented in Section 3.1.6 indicates that this elevated slab temperature increased reactivity by 60% in comparison to slabs at 22°C.

Figure 9. Effect of decrease in slab moisture due to water evaporation on NO oxidation rate (photoreactor vapor density held constant).

In this study, the peak NO oxidation rate was observed at 2% decrease in slab moisture. Under field condition a different peak would be observed. This difference would arise because water content varies throughout the depth of a concrete pavement; therefore, the decrease in moisture at the pavement surface would differ from the decrease in moisture throughout the entire slab. Overall, the findings presented in Figure 9 complicate recommendations for field application of TiO₂-containing pavements. On the basis of relative humidity, areas with sustained periods of low humidity would be recommended for application. It would be assumed that mitigation of NO pollution would continue as long as relative humidity remained low. However, sustained low humidity would also cause evaporation of water contained in the pores of the slab. Based on the data presented, a photocatalytic concrete pavement could be expected to remove NO initially; however, over time NO oxidation would decrease and the benefits would be lost. If TiO₂-containing pavement is to be applied in the field to mitigate NO pollution,

this complicating factor requires further investigation and methods to maintain moisture in the pavement may need to be developed.

3.1.6. Slab Temperature

Figure 10 displays the effect of temperature on NO oxidation rate on axes of NO oxidation rate versus temperature (Figure 10a) and $\ln(\text{NO oxidation rate})$ versus the inverse of temperature (Figure 10b). Linear regression of this data found a R^2 value of 0.880. A model utility test rejected a null hypothesis that slope equaled $0 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}\cdot^\circ\text{C}^{-1}$ with confidence in excess of 99.99% ($t = 8.963$, $df = 12$). As noted in Section 2.4.2, tests which occurred at slab temperatures below 22°C presented the possibility of error due to water condensation. Linear regression of data points above 22°C found a slope of $0.459 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}\cdot^\circ\text{C}^{-1}$ ($R^2 = 0.725$, $n = 7$); for data points below 22°C the slope was $0.252 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}\cdot^\circ\text{C}^{-1}$ ($R^2 = 0.417$, $n = 6$). A pooled-variance t -test of a null hypothesis that the difference between these two slopes was 0 (i.e., $H_0: B_1 - B_2 = 0$) indicated that the slopes were not significantly different ($t = 0.967$, $df = 9$, $p = 0.359$). Although the values of the slopes differ, the data collected did not support a claim that this difference was significant.

Figure 10. Effect of temperature on NO oxidation rate.

The effect of temperature on NO oxidation rates has not been studied in previous photoreactor studies; therefore, comparison with other data sets was not possible. Other photocatalytic pavement studies that do make statements in regard to the impact of temperature on oxidation rates are often vague. In most instances these studies assert that the oxidation rate increases with an increase in temperature (Beeldens et al., 2011) and that only large differences in temperature (i.e., summer vs. winter) are significant (Dylla et al., 2011). In addition to being vague, the literature also is contradictory and one source reported a decrease in oxidation rate with increased temperature (Chen & Chu, 2011). One aqueous photocatalysis publication, Herrmann (1999), does provide useful insight for this study. It stated that in the range of 20–80°C, activation energy was negligible and was not a rate limiting step. Furthermore, at temperatures below 0°C, the apparent activation energy of the photocatalyst increased leading to a decrease in oxidation rate.

The Arrhenius equation offers an empirical relationship between a reaction rate constant (k), temperature (T), pre-exponential factor (A), activation energy (E_a), and the universal gas constant (R):

$$k = A \cdot e^{\frac{-E_a}{R \cdot T}}$$

Using log properties, this equation can also be expressed as follows:

$$\ln k = \frac{-E_a}{R} \left(\frac{1}{T} \right) + \ln A$$

When graphed on axes of $\ln(\text{NO oxidation rate})$ and the inverse of temperature ($1/T$), reactions that follow the Arrhenius equation exhibit a linear relationship. Figure 10b does not display this type of relationship. Overall, while the information discussed in this section partially explains the observations; it would appear that given the complexity of photocatalytic pavement materials, other factors also influenced the reported observations.

4. Conclusions

Photocatalytic pavements offer a novel technological option to mitigate NO_x pollution. In order for these pavements to be adopted by potential stakeholders, information is needed that documents the NO oxidation rate under varied environmental conditions. A positive correlation was observed between NO oxidation rate and influent NO concentration. Comparison of this study with Hüsken and Brouwers (2008), Hüsken et al. (2009) and Ballari et al. (2010), who also studied cementitious photocatalytic pavements, found no significant difference in the slope of regression lines through this data. However, a significant difference in slope was observed in comparison with Murata et al. (2000). A positive correlation was also observed between NO oxidation rates and UV-A irradiance ($R^2 = 0.996$). Comparison of this study with Hüsken et al. (2009) found no significant difference in the slope of regression lines through this data. A significant difference in slope was observed in comparison with Murata et al. (2000). A correlation was not observed between NO oxidation rates and flow rate. This same conclusion was reached with analysis of data from Hüsken and Brouwers (2008) and Hüsken et al. (2009). A negative correlation was observed between NO oxidation rate and relative humidity. In contrast with evaluations for UV-A irradiance and NO concentration, no significant difference was found with comparison of this study to Murata et al. (2000). A significant difference in slope was observed between this study and Hüsken and Brouwers (2008) and Hüsken et al. (2009). Decrease in slab moisture, a variable not investigated in prior work, was found to affect NO oxidation rates. At losses of 0–2% of saturated mass, a positive correlation was observed; whereas, at losses greater than 2% a negative correlation was observed. A positive correlation was documented for slab temperature. This finding contrasts previous assertions which considered this variable insignificant.

Overall, it can be concluded that photocatalytic mortar slabs manufactured with TX Active pavement are highly sensitive to changes in environmental variables. NO oxidation rates observed in this study ranged from 9.8–64 nmol·m⁻²·s⁻¹. Furthermore, significant differences were found by comparison to other

studies. Therefore, if a potential stakeholder is considering use of this technology to mitigate NO_x emissions, careful preliminary work should be undertaken to both evaluate the environmental conditions of the test site and the properties of the selected photocatalytic material.

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Black and White Versions of Color Figures

Figure1. Photocatalytic oxidation of NO and NO₂ by pavement containing TiO₂ (partially adapted from Ballari et al., 2011).

Figure 2. Diagram of experimental apparatus (partially adapted from Ballari et al., 2011).

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644 **Figure 3. Photograph of photoreactor and mortar slab (optical window removed to facilitate viewing).**